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**Smith & Loveless, Inc.®** **14040 West Santa Fe Trail Drive Lenexa, Kansas 66215-1284**

### **VACUUM PRIMED NON-CLOG PUMPS SECTION INDEX**



#### **4" – PUMPS**

#### **Pump Assembly Drawings & Curves**





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## **4" – PUMPS**



## **Pump Assembly Drawings & Curves**





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### **8" – PUMPS**



• 8C4V / 8D4V Pumps, Pump Curve, 875 RPM 62L199

## **12" – PUMPS**

### **Pump Assembly Drawings & Curves**



## **50 Hz Pump Curves**



## **Vacuum Priming Schematic**



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**14040 West Santa Fe Trail Drive Lenexa, Kansas 66215-1284** **X-PELLER®** Pump with Mono-Port Impeller Notes on Design July, 2012 Page 1

#### **NOTES ON DESIGN FOR X-PELLER® PUMP**

Smith & Loveless has raised non-clog pumping to a new level with the Smith & Loveless **X-PELLER®** pump design. In addition to all of the features and associated benefits incorporated in the traditional Smith & Loveless pump design (such as solid stainless steel shaft, oversized bearings, full diameter impeller shrouds, tapered shaft, long life seal, etc.), Smith & Loveless **X-PELLER®** pumps with the patented mono-port hydraulic design give a new meaning to the term "non-clog".

The unique mono-port, single passageway, "V" vane design virtually eliminates the opportunity for pump solids to hang up in the impeller. Stringy material, which used to hang up on the leading edges of the vanes of twoport impellers, now has no place to lodge, and passes freely through the pump. Passageway openings through the impeller have a cross-section of at least 10.6 square inches, and clearance to pass a three-inch (3") sphere, so large solids are not a problem either.

A typical two-port pump impeller includes a single suction eye having two ports opening into opposing expanding chambers. The ports have smaller openings than the single, axial opening of the suction eye, due to the fact that each port handles one-half of the total flow. Solids, which are small enough to enter the suction eye axial opening, may be too large to pass through either port, eventually significantly plugging the impeller. Stringy material may have one end drawn into one port and the other end drawn into the other port. Thus, the material may be draped around the base edge of an impeller vane. More stringy materials can build up this way, and the ports can become substantially clogged. Furthermore, even if the materials impeding flow through the ports do not completely clog the impeller, the buildup of these materials may cause the pump impeller to be out of balance, resulting in pump vibration.

To alleviate these problems, a mono-port centrifugal pump impeller is used in the **X-PELLER®** pump, making it ideal for solids handling, i.e., handling liquids with entrained solid matter. The mono-port impeller design eliminates clogging in solids-handling applications, particularly when handling stringy materials.

The single radial passage through the impeller is essentially the same size as the opening of the suction eye of the impeller, so that any object entering the pump will pass completely through the impeller without clogging.

There are no impeller parts for stringy material to hang on, which would restrict flow through the impeller.

The **X-PELLER®** is ideally suited for pumping applications for prisons, hospitals, mental institutions, and other type applications where high concentrations of large or stringy solids might be expected. The **X-PELLER<sup>®</sup>** is also ideally suited for sludge pumping applications, such as RAS or WAS flows in a treatment plant. As with all Smith & Loveless pumps, a fresh water seal system is recommended when pumping sludge.

Field experience has shown that plugging is not often a problem with six-inch (6") pumps, and virtually unheard of in pumps eight inches (8") and larger, when handling raw sewage. It is mostly in the four-inch (4") size pumps that plugging has been traditionally a problem. This is due in part to the lower flows involved, as well as the smaller geometry. The **X-PELLER®** pump eliminates the catch points for stringy materials and passes the entire flow through a single port opening, with a cross-sectional area of up to fifty percent (50%) greater than that of the passageway of a two-port impeller. These features greatly improve its clogging resistance.

Another feature of the **X-PELLER®** design is it may be trimmed to a different diameter without having to rebalance the impeller assembly. This is unique to Smith & Loveless, as our competitors' single port design must be balanced after trimming, and re-balanced after retrimming. In addition, the balance of the **X-PELLER®** is not only static and mechanically dynamic, but also hydraulic. This is important. It is one thing to have an impeller, which will spin without vibration on a dry test stand, but quite another thing to operate without vibration when subjected to the hydraulic forces of a centrifugal pump. The **X-PELLER®** is balanced to take all of these dynamic forces into consideration. Because of its unique vane shape and hydraulics, the **X-PELLER®** has a somewhat different vibration signature than the standard two-port design. This is entirely normal, and should not be cause for alarm. Vibration with the **X-PELLER®** design is within generally accepted industry standards for non-clog pumps.

There is another advantage to the **X-PELLER®** pump, inherent in the mono-port hydraulic design. The pump performance curve, or impeller line, has a rather steep downward slope. This is important in low flow pumping applications (which usually account for most clog-prone situations). By having a steep pump curve, variations in

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head on the pump do not have as significant an effect on the flow rate of the pump as they do on a pump with a flatter performance curve. Changes in wet well level, or force main conditions, will not be as apt to cause the pump to back up to Shut-Off or Run-Out and Over-Pump or overload the pump motor. This is a good feature to have in low flow pumping applications.

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The **X-PELLER®** design offers good insurance against possible clogging problems when selecting pumps for new installations, especially those with large solids to handle. For existing problem applications where twoport impellers have proven inadequate, the **X-PELLER®** makes an excellent retrofit solution. Replacement **X-PELLERs®** can be retrofitted to most Smith & Loveless four-inch (4") 2-frame pumps and some six-inch (6") 3 frame pumps – both flooded suction and vacuum primed. In addition, the **X-PELLER®** is available for retrofitting into several of our competitors' four-inch (4") and sixinch (6") pump models. Consult the Retrofit Department for specific applications.

Where plugging has been a problem or may be expected to be a problem, and for all large solids handling operations, the **X-PELLER®** is the solution.

Vacuum Primed Pump Stations Notes on Force Main Design Design Factors July, 2012 Page 1

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## **DESIGN FACTORS – NOTES ON FORCE MAIN DESIGN**

Under certain unusual conditions, the wet well mounted pump station force main requires special provisions to prevent loss of prime of the station.

Force mains for wastewater discharged from a wet well mounted pump station may be of iron, PVC or other material generally used in the area. Conventional design criteria for force main layout, anchoring, etc., should be followed. It is especially important to provide air release or air/vacuum valves at all high points in the force main.

The station has two rubber-seated check valves in the discharge piping. These valves must be seated airtight when the vacuum pump comes on or else the vacuum pump will suck air through the check valves and the station will not prime. For most installations this is not a problem; if we have a force main, such as shown in Figure 1, where the force main is of considerable length, (at least 150 feet), there is a static head on the check valves, and a large volume of sewage in the force main. Since the force main runs uphill, the sewage cannot flow out of the force main, and there is a static head on the check valves to keep them seated. If there is some sewage leaking back through the check valve, the length of the force main creates enough capacity that it takes a considerable length of time for the sewage to drain back through the check valve and create a loss of prime condition. Since the force main is long, we also have the advantage that the sewage flowing back through the check valve into the wet well will refill the wet well and bring the pump on before the force main is empty. Therefore, when we have a long force main running uphill as shown in Figure 1, we do not have a priming problem because of air being sucked through the check valves.





**Figure 3**

When we have a short force main running uphill from the station, as shown in Figure 2, we can have a priming problem.

If the force main is less than approximately 150 feet long, there is not much reserve capacity in the force main. If one of the discharge check valves is allowing the sewage in the force main to seep back into the wet well, it is possible that the force main will empty back into the wet well before the level in the wet well rises to bring a pump on. Since the check valves do not seal against air, the pump loses its prime, and when the vacuum pump comes on to prime either pump, it sucks air through the force main and leaking check valve and cannot prime the pump.

To prevent this problem, we recommend installing a third check valve in the common discharge from the station. This check valve should be installed in the horizontal run of pipe inside the wet well. The check valve is shipped loose, and is installed in the force main by the installing

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contractor. The reason for the third check valve is that this gives a double checking action on both pumps. It is very unlikely that both check valves will be hung up on a mop string or piece of paper at the same time, thus creating a loss of prime.

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We can also have a priming problem if we have a long force main running downhill from the station as shown in Figure 3. In this type of installation, after the pump shuts off, the force main empties out by gravity, allowing air to get on the force main side of the check valve. Here again, the pump loses prime, and when the vacuum pump comes on and tries to prime the pump, it sucks air through the empty force main and leaking check valve. To prevent this from happening, we recommend that the force main be installed with the last 50 feet of pipe running uphill, as shown in Figure 3. The invert of the outfall should be at least two pipe diameters above the low point in the force main. This creates a water trap, and when the pump shuts off, air cannot get into the force main, allowing the contents to empty out by gravity. If it is not possible to run the last 50 feet of force main uphill, as shown in Figure 3, then an elbow can be installed on the end of the force main to create the same water trap effect.

The installation shown in Figure 4, a short force main (less than 150 feet) running downhill from the station also creates a possible priming problem. Here we have the possibility of both the force main emptying out by gravity, and the check valve allowing sewage to seep back through the pump. If at all possible, the force main should be extended down into the wet well, and exit at an elevation so that the force main can run uphill from the station. Refer to the dotted line of Figure 4 which shows the recommended force main installation. Here again, if it is not possible to run the force main uphill from the station, an elbow can be installed at the end of the force main. This creates a water trap effect, and does not allow air to enter the force main. If air cannot enter the force main, the sewage cannot flow out by gravity. Once this has been done, we have the same condition that we have in Figure 2. A third check valve must now be installed in the horizontal run of force main in the wet well. This check valve gives a double checking action and prevents the contents of the force main from seeping back through the pump, causing a loss of prime.



#### **THE FOLLOWING INFORMATION IS GIVEN FOR GENERAL GUIDELINES**

The force main is considered to run uphill from the station if the invert of the outfall is at least two pipe diameters above the low point of the force main. This creates the air-trap effect, so that the sewage will not flow out of the force main by gravity.

The force main is considered to be a short force main, and requires a third check valve, if the volume of the force main is less than the volume of the wet well between the "On" and "Off" levels. Assuming a wet well "On" "Off" capacity of 100 gallons and the force main is four-inch with a capacity of approximately seven-tenths gallon per foot, the force main would have to be approximately 150 feet long to have a capacity of 100 gallons. The reasoning behind this particular design requirements is that if the check valve should seep and allow the sewage to run back through the pump and into the wet well, there will be enough contents in the force main to bring the wet well back up to the "On" position, and the pump will start before the force main empties. As a minimum, the elevation between the "Low-Level Off" float switch and the "Low-Level On" float switch is such that the volume between switches is equal to the pump capacity. If the switches are set farther apart, more capacity is required in the force main.

Of course, in all cases, the outfall must be at a higher elevation than the lowest water level in the wet well. Otherwise, siphoning the wet well dry will cause loss of prime through the suction lines.

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The above examples should cover every installation for a wet well mounted pump station. If you have an unusual condition that is not covered by the examples given above, consult the factory, and we will give you a special recommendation for your application.

#### **PRIMING LOCK LOOP**

Another solution that is suitable for any of the problem force mains described previously is a priming lock loop. The purpose here is to form a return loop in the force main, either inside or just outside the wet well. The bottom of the loop must be below the low level "Off" elevation (see Figure 5). This prevents the entire contents of the force main from returning by gravity to the wet well if the check valve does not seat. There will still be enough liquid in the pipe to prime the pump. On force mains that run horizontal or downhill from the station, the last few feet of the force main should run uphill to create a water trap effect in the force main.



**Figure 5**



Vacuum Primed Pump Stations Priming Lock Loop Installation Drawing 87B289 – 4" Piping July, 2012 Page 1





Vacuum Primed Pump Stations Priming Lock Loop Installation Drawing 87B293 – 6" Piping July, 2012 Page 1





Vacuum Primed Pump Stations Suction Pipe Supports Drawing 87B290





Vacuum Primed Pump Stations Installation Details Drawing 87B650 July, 2012 Page 1





Vacuum Primed Pump Stations Typical Wet Well Level Settings Drawing 87B721 4" and 6" Pumps July, 2012 Page 1





Vacuum Primed Pump Stations Recommended Pipe Restraint Detail (Vertical Discharge Pipe) Drawing 87A622 July, 2012 Page 1





Vacuum Primed Pump Selection Chart Drawing 62L189 – 4" Pumps 6B3B / 6B3X / 8D4D July, 2012 Page 1





**14040 West Santa Fe Trail Drive Lenexa, Kansas 66215-1284** Suction Line Considerations 8D4V / 12D6V Pumps July, 2012 Page 1

#### **SUCTION LINE CONSIDERATIONS 8D4V & 12D6V PUMPS**

#### **MAXIMIZING SUCTION LIFT CAPABILITY**

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In addition to providing well supported and braced, leaktight suction lines for vacuum primed pumps (reference Drawing 87B290 or 87B650), it is equally important to provide good hydraulic conditions to insure the optimum suction lift performance.

Suction lines should be as large in diameter as practical without reducing the velocity below the minimum for carrying solids, usually 2.0 fps. Refer to the recommended ranges on the Smith & Loveless pump curves as a guideline. Avoid unnecessary bends or ells, and horizontal runs of pipe, to minimize friction losses. Friction from any piping other than the straight downward run shown in the catalog drawings must be deducted from the allowable suction lift.

For 4" and 6" pumps, the bottom of the suction pipe should be approximately 6" above the floor of the wet well and a minimum of 12" below the "Off" level setting of the controls. For 8" and 12" pumps, refer to the following section, addressing them specifically. When using these distances, a bell or flare inlet is not necessary. A foot valve is not recommended for normal applications of vacuum primed pumps.

Liquid temperatures above about 85 degrees F. will cause a reduction in allowable suction lift due to the increase in vapor pressure. Consult the Factory in these cases.

#### **DERATING FOR ALTITUDE**

Most Smith & Loveless vacuum primed pump curves show the maximum allowable static suction lift, either as a note (Maximum Suction Lift at M.S.L.  $-20$ ) or as a family of curves delineating the maximum, if below 20'. These values are based atmospheric pressure at Mean Sea Level and on the vertical distance measured from the "Off" control level setting in the wet well up to the station baseplate or top of the wet well where the station sits.

The maximum allowable static suction lift must be derated for altitude at higher elevations. For every 1000' of altitude, it is necessary to derate the allowable static suction lift by 1.0', to account for the decrease in atmospheric pressure. Therefore, a pump that is capable

of 20' of static suction lift at sea level is only good for 15' at 5000' elevation.

#### **8D4V / 12D6V PUMPS**

The suction pipe sizing and suction lift ratings of the 8D4V and 12D6V pumps are determined differently than for other Smith & Loveless vacuum primed pumps. In addition, some of the suction piping dimensions are different, all due to the high flows involved with these bigger pumps.

The chart with Max and Min flows on Page 3 will assist in selection of possible suction pipe sizes, based on the design flow rate of the pump (or the single pump run-out flow rate for multiple pump installations). It would be good to consider something larger than the absolute minimum allowable size, to keep losses down and suction lift up. This chart also will give the proper clearance distance from the bottom of the suction pipe to the bottom of the wet well ("C") to provide good solids collection, and the minimum submergence of the suction inlet ("S") to avoid vortexing and drawing in air. These numbers are based on Hydraulic Institute recommendations.

To determine the maximum static suction lift (the distance from the top of the wet well or baseplate of the station down to the "Low Level Off" elevation), use the appropriate chart on Page 4. The bottom chart is only for the 1760 RPM 8D4V pump, which has a flow conditioner. The top chart is for the other 8D4V pump speeds and all of the 12D6V pumps. These charges take into account the suction line friction, velocity and entry losses.

Find the intersection between the plotted line for the suction size selected and the vertical line for the maximum flow rate expected through the pump. From this intersection, read the maximum static suction lift horizontally from the scale on the left. Note that large suction lines allow more suction lift. Adjust your suction pipe selection if necessary.

The maximum static suction lift is based on using Schedule 80 PVC suction lines and atmospheric pressure at sea level. For higher altitudes, derate the maximum static suction lift by 1.0' per 1000 feet above sea level.

#### **ENGINEERING DATA Smith & Loveless, Inc.® 14040 West Santa Fe Trail Drive Lenexa, Kansas 66215-1284**

Suction Line Considerations 8D4V / 12D6V Pumps July, 2012 Page 2

**EXAMPLE:** *For 3000 GPM, using the 8D4V pump at 1170 RPM, at 2050' elevation, the chart on Page 2 allows 14" and larger suction lines. Try the 14" first. From the top chart on Page 3, a 14" suction at 3000 GPM is good for 16.3' SSL. Derating that by 1'/1000 ft. altitude, we get 14.3' Max. If we go to 16", the chart allows 17.4', which, after derating, leaves 15.4'. Doing the same with 18" pipe results in 18.0' - 2' = 16.0' Max. and 20" gives us 18.4' - 2' = 16.4'. We see that larger suctions allow more suction lift, but at a diminishing rate. Do not skimp on suction size. Select a suction pipe size that gives more than the required SSL, but is still economical.*



SUCTION LINE CONSIDERATIONS - 8D4V & 12D6V PUMPS







Suction Lift Limits 8D4V & 12D6V Pumps January, 2011

#### SUCTION LIFT LIMITS - 8D4V & 12D6V PUMPS









Vacuum Primed Pump Performance Curve 62L139 Constant Speed 4B2C Turbo Pump 1170 RPM July, 2012





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(See Factory Order)<br>(See Factory Order)



Pump Assembly Drawing 4C2B / 4C2D / 4C2X Drawing 87B454 July, 2012





Vacuum Primed Pump Performance Curve 62L18 Constant Speed Non-Clog Pump 4B2B / 4C2B – 1760 RPM July, 2012





Vacuum Primed Pump Performance Curve 62L17 Constant Speed Non-Clog Pump 4B2B – 1170 RPM July, 2012





Vacuum Primed Pump Performance Curve 62L16 Constant Speed Non-Clog Pump 4B2B – 875 RPM July, 2012



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Vacuum Primed Pump Performance Curve 62L9 Constant Speed Non-Clog Pump 4B2D – 1760 RPM July, 2012





Vacuum Primed Pump Performance Curve 62L8 Constant Speed Non-Clog Pump 4B2D – 1170 RPM July, 2012





Wet Well Mounted Pump Station Performance Curve 62L185 Constant Speed Non-Clog Pump **X-PELLER®** Impeller 4B2X / 4C2X – 1760 RPM July, 2012





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**14040 West Santa Fe Trail Drive Lenexa, Kansas 66215-1284** Wet Well Mounted Pump Station Performance Curve 62L184 Constant Speed Non-Clog Pump **X-PELLER®** Impeller 4B2X – 1170 RPM July, 2012





Wet Well Mounted Pump Station Performance Curve 62L183 Constant Speed Non-Clog Pump **X-PELLER®** Impeller 4B2X – 875 RPM July, 2012





Pump Assembly Drawing 4B3B Drawing 87B456 July, 2012









Pump Assembly Drawing 4D3B Drawing 87B458 July, 2012




Vacuum Primed Pump Performance Curve 62L146 Constant Speed Non-Clog Pump 4B3B / 4C3B / 4D3B – 1760 RPM





Vacuum Primed Pump Performance Curve 62L145 Constant Speed Non-Clog Pump 4B3B / 4C3B – 1170 RPM July, 2012







Vacuum Primed Pump Performance Curve 62L182 Constant Speed Non-Clog Pump 4D4B – 1760 RPM July, 2012









Pump Assembly Drawing Drawing 87B469





Vacuum Primed Pump Performance Curve 62L33 Constant Speed Non-Clog Pump 6B3B / 6C3B / 6D3B – 1760 RPM July, 2012





Vacuum Primed Pump Performance Curve 62L32 Constant Speed Non-Clog Pump 6B3B / 6C3B – 1170 RPM July, 2012





Vacuum Primed Pump Performance Curve 62L31 Constant Speed Non-Clog Pump 6B3B – 875 RPM July, 2012





Vacuum Primed Pump Performance Curve 62L299 Constant Speed Non-Clog Pump 6B3X / 6C3X / 6D3X – 1760 RPM July, 2012





Vacuum Primed Pump Performance Curve 62L297 Constant Speed Non-Clog Pump 6B3X / 6C3X – 1170 RPM July, 2012





Vacuum Primed Pump Performance Curve 62L295 Constant Speed Non-Clog Pump 6B3X – 875 RPM July, 2012



## **ENGINEERING DATA**

**Smith & Loveless, Inc.®** **14040 West Santa Fe Trail Drive Lenexa, Kansas 66215-1284** Vacuum Primed Pump Performance Curve 62L195 Constant Speed Non-Clog Pump 6D4V – 1760 RPM July, 2012



## **ENGINEERING DATA Smith &**

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**14040 West Santa Fe Trail Drive Lenexa, Kansas 66215-1284** Vacuum Primed Pump Performance Curve 62L194 Constant Speed Non-Clog Pump 6D4V – 1170 RPM July, 2012





**Lenexa, Kansas 66215-1284**

Vacuum Primed Pump Performance Curve 62L193 Constant Speed Non-Clog Pump 6C4V / 6D4V – 875 RPM July, 2012







Vacuum Primed Pump Performance Curve 62L157 Constant Speed Non-Clog Pump 8C4D / 8D4D – 1170 RPM July, 2012





Vacuum Primed Pump Performance Curve 62L156 Constant Speed Non-Clog Pump 8C4D / 8D4D – 875 RPM July, 2012





Vacuum Primed Pump Performance Curve 62L201 Constant Speed Non-Clog Pump 8D4V – 1760 RPM July, 2012





**Lenexa, Kansas 66215-1284**

Vacuum Primed Pump Performance Curve 62L200 Constant Speed Non-Clog Pump 8D4V – 1170 RPM July, 2012





Vacuum Prime Pump Performance Curve 62L199 Constant Speed Non-Clog Pump 8C4V / 8D4V – 875 RPM July, 2012





Vacuum Primed Pump Performance Curve 62L202 Constant Speed Non-Clog Pump 12D6V – 1170 RPM July, 2012





Vacuum Primed Pump Performance Curve 62L203 Constant Speed Non-Clog Pump 12D6V – 875 RPM July, 2012





Vacuum Primed Pump Performance Curve 62L211 Constant Speed Non-Clog Pump 12D6V – 700 RPM July, 2012





Vacuum Primed Pump Performance Curve 62L206 Constant Speed Non-Clog Pump 12D6V – 585 RPM July, 2012





Vacuum Primed Pump Performance Curve 62L161 Constant Speed Non-Clog Pump 4B2B – 1470 RPM July, 2012





Vacuum Primed Pump Performance Curve 62L160 Constant Speed Non-Clog Pump 4B2B – 980 RPM July, 2012





Vacuum Primed Pump Performance Curve 62L155 Constant Speed Non-Clog Pump 4B2D – 1470 RPM July, 2012





Vacuum Primed Pump Performance Curve 62L154 Constant Speed Non-Clog Pump 4B2D – 980 RPM July, 2012





Vacuum Primed Pump Performance Curve 62L163 Constant Speed Non-Clog Pump 4B3B / 4C3B / 4D3B – 1470 RPM July, 2012





Vacuum Primed Pump Performance Curve 62L162 Constant Speed Non-Clog Pump 4B3B / 4C3B – 980 RPM July, 2012





Vacuum Primed Pump Performance Curve 62L165 Constant Speed Non-Clog Pump 6B3B / 6C3B / 6D3B – 1470 RPM July, 2012





Vacuum Primed Pump Performance Curve 62L164 Constant Speed Non-Clog Pump 6B3B / 6C3B – 980 RPM July, 2012





Vacuum Priming Diagram Vacuum Primed Pump Station Drawing 87B503 July, 2012





Vacuum Priming Diagram Vacuum Primed Pump Station Drawing 87B504 July, 2012

